

HYDROGEN REFUELLING STATION CALIBRATION WITH A TRACEABLE GRAVIMETRIC STANDARD

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HYDROGEN REFUELLING STATION CALIBRATION

Related European Programs

- This work has been realized within two European projects

MetroHyVe – EURAMET EMPIR call



FCH-JU : FCH / OP / 196 : “Development of a Metering Protocol for Hydrogen Refuelling Stations”



HYDROGEN REFUELLING STATION CALIBRATION

Road map of the presentation



- ❑ **Background regarding HRS in Europe**
- ❑ **Basic operating principle of a HRS station**
- ❑ **Test protocol for HRS calibration (on-site) and primary gravimetric standard.**
- ❑ **Results from on-site measurements with the primary traceable gravimetric standard.**
- ❑ **Conclusions and perspectives**

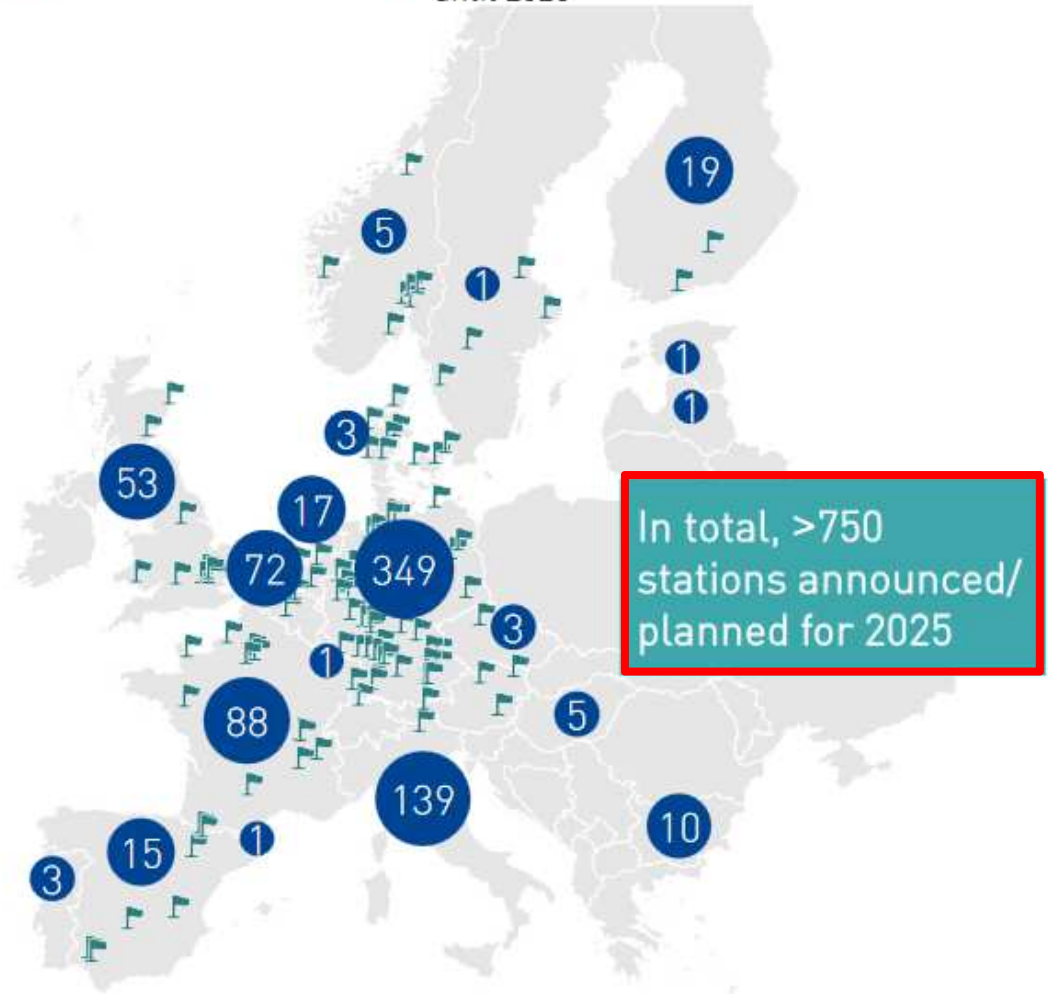
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Background regarding HRS in Europe







- H2 HRS growth in Europe







Current and planned HRS in Europe

 HRS in operation²
 Number of HRS announced and/or planned until 2025



FCEV share in respective segment

		2030	2050
Small cars		2%	22%
Larger cars		5%	39%
Taxis		14%	61%
Vans/LCVs		8%	49%
Buses		6%	45%
Trucks		1%	35%

Small cars		0%	14%
Larger cars		2%	28%
Taxis		8%	57%
Vans/LCVs		3%	30%
Buses		2%	25%
Trucks		<1%	21%

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Background regarding HRS in Europe

- Why H2 dispensers are not certified yet?
 - Flow meters are not approved according to OIML R139 due to the absence of testing facilities (H2, 700 bar, ...)
 - OIML R139-2014 was not adapted for hydrogen dispensers

The standard has been revised in 2017-2018.

*New version issued on **Oct 2018**.*

→ Therefore, short-term solution for the approval H2 dispensers is necessary for the ramp-up of the HRS network in Europe

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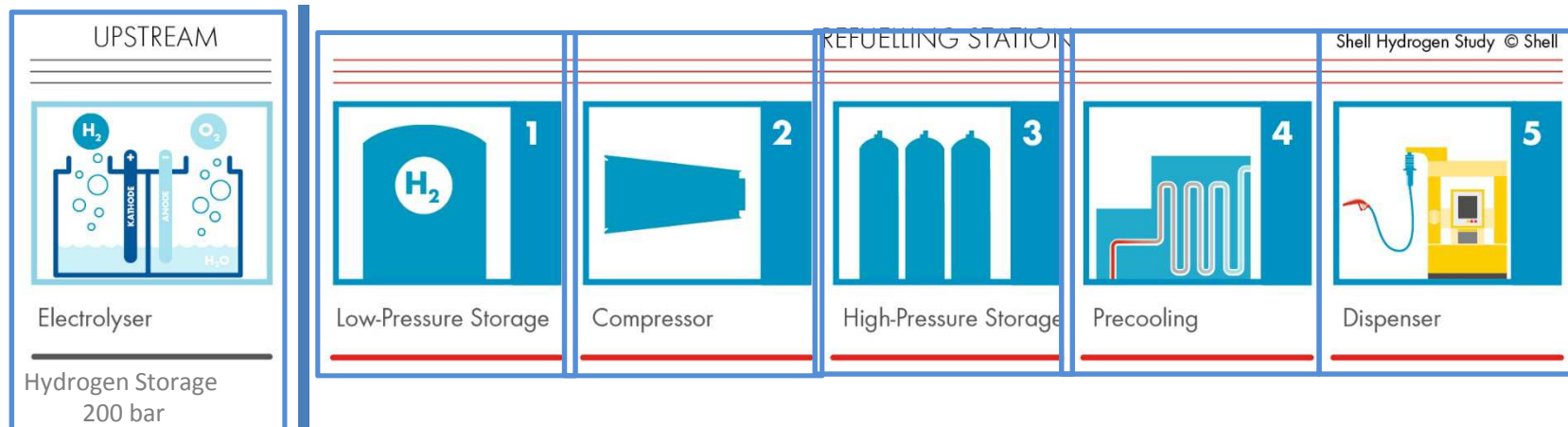
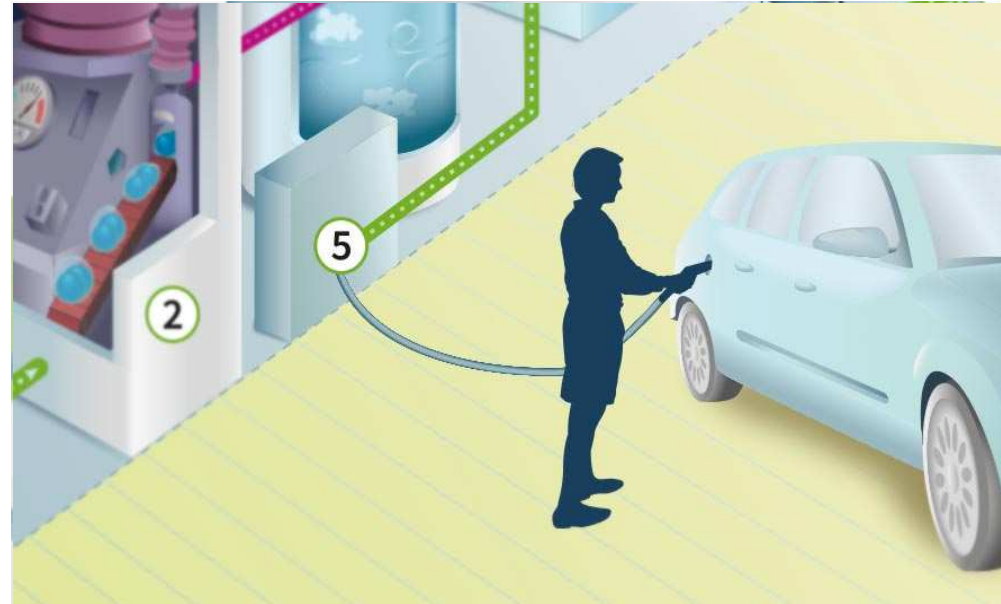
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Basic operating principle of a HRS station

- Basic principle and listing of the component:



Photo courtesy of the California Fuel Cell Partnership



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Test protocol for HRS calibration (on-site)

- Revision of the OIML R139 standard for gaseous dispensers
 - OIML R139 revision initiated in **March 2017** to include specificities of Hydrogen dispensers
 - Accuracy classes have been largely discussed and revised:
 - **Class 2 & Class 4** have been created for hydrogen service

Table 1 - MPE values

Accuracy class		MPE for the meter [in % of the measured quantity value]	MPE for the complete measuring system [in % of the measured quantity value]	
			at type evaluation, initial or subsequent verification	in-service inspection under rated operating conditions
For general application	1.5	1	1.5	2
For hydrogen only	2	1.5	2	3
	4	2	4	5

- In principle: **Class 2** is accepted for future stations, whereas **Class 4** is tolerated for existing stations

How to test a complete measuring system?

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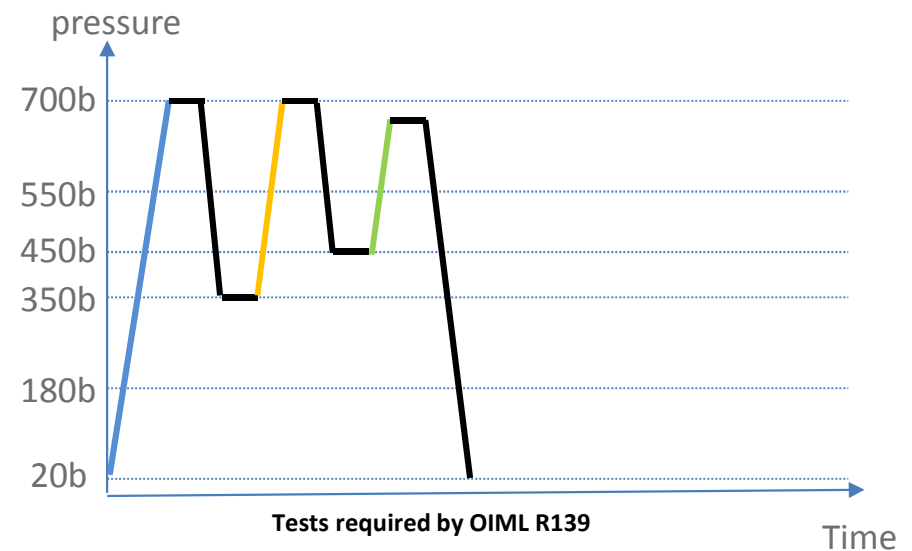
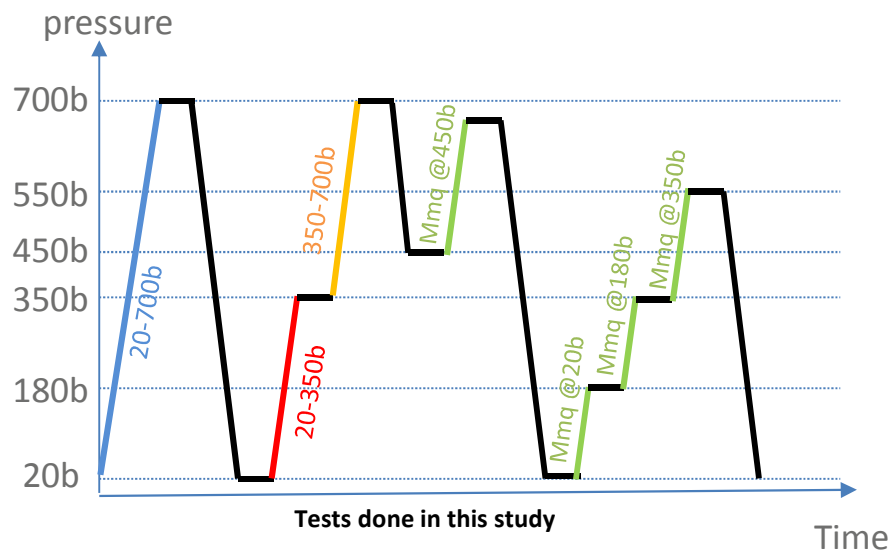
Test protocol for HRS calibration (on-site)

- Accuracy tests based on OIMLR139-2018

- Full series of tests:

- 1 full fillings 20-700 bar Automatic stop
- 1 partial fillings 20-350 bar Manual stop
- 1 partial fillings 350-700 bar Automatic stop
- 4 MMQ fillings 1Kg Manual stop
with different starting pressure (450 bar - 20 bar - 180 bar - 350 bar)

- This series of tests is performed **4 times**



Which kind of technologies have been tested ?

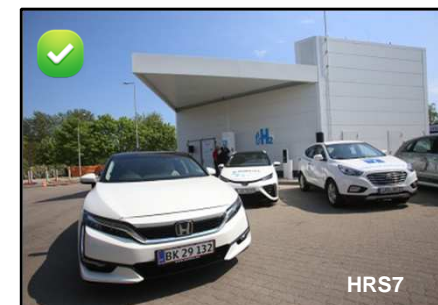
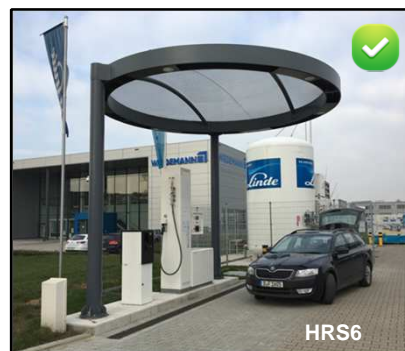
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Test protocol for HRS calibration (on-site)

• HRS technologies

- compressed gas or liquid hydrogen (cryo pump) & compressed gas (ionic compressor)
- MFM located in the station, which can be far away from the dispenser / 3 different Coriolis manufacturers

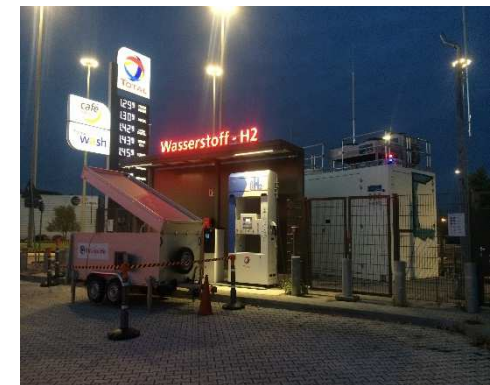
• HRS location (France, Germany (mainly) and Netherland)



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primary gravimetric standard (Air Liquide)

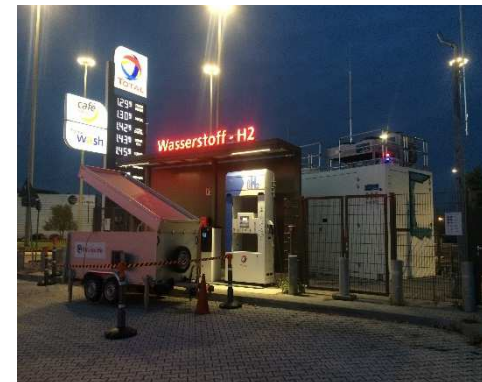
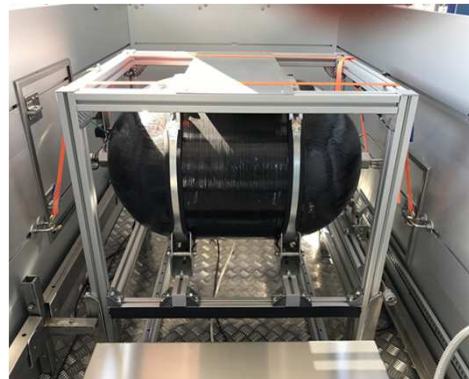
- **Main characteristics and design (Air Liquide + Cesame Exadebit)**
 - **High precision scale:** 150 kg resolution 0.2g, Ex-certified
 - **Composite tank type 4** of 104L (i.e. 4,0 Kg of Hydrogen at 700 bar, 15°C)
 - **Mobile** test bench (trailer) to be moved on each HRS
 - Trailer walls, doors and roof serve as **protection against wind**
 - Protection against fire (**TPRD**)
 - Possibility to remove the scale for transportation
 - Valve panel to **inert tank with N2** for transportation
 - Independent **vent stack** for depressurization of the tank



HYDROGEN REFUELLING STATION CALIBRATION

primary gravimetric standard (Air Liquide)

- **Testing device designed and manufactured by Air Liquide (with Cesame Exadebit)**
 - Certified by PTB (March 2018) as first reference standard for calibration, conformity assessment and verification of hydrogen refueling dispensers
 - Also accepted by LNE (France) and NMI Certin (Netherlands)
 - Fulfills metrological requirements as per OIML R139-2018
 - Uncertainty $U < \frac{1}{3} \text{ MPE} = 0,3\%$
 - Uncertainty budget defined in collaboration with PTB / LNE / Cesame Exadebit
- **CE approval**
 - Issue: tank is not designed as per PED, but **EC79** (on-board storage)
 - Long process with the Notified Body to get a Conformity Assessment according to PED
- **Testing equipment conform to Ex rules**



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- ❑ **Results from on-site measurements with the primary traceable gravimetric standard.**
- ❑ Conclusions and perspectives

HYDROGEN REFUELLING STATION CALIBRATION

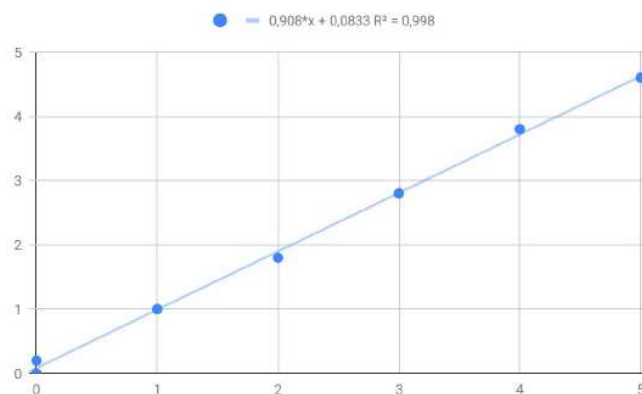
Results from on-site measurements with gravimetric standard

- **Typical planning of a testing week:**

- Installation: 2-3h
- Scale verification: 30 min
- Accuracy test: 3 days
- De-installation: 2-3h

- **Scale verification**

- Warm-up time required of about 1h30-2h
 - Scale must remain powered during nights to save time each morning
- Verification using reference weights: 1 Kg / 2Kg / 4 Kg / 5 Kg:
 - One full verification on the 1st day
 - Then light verification each morning
- Linear correction brought to mass measurements
 - Based on scale deviation measured each day

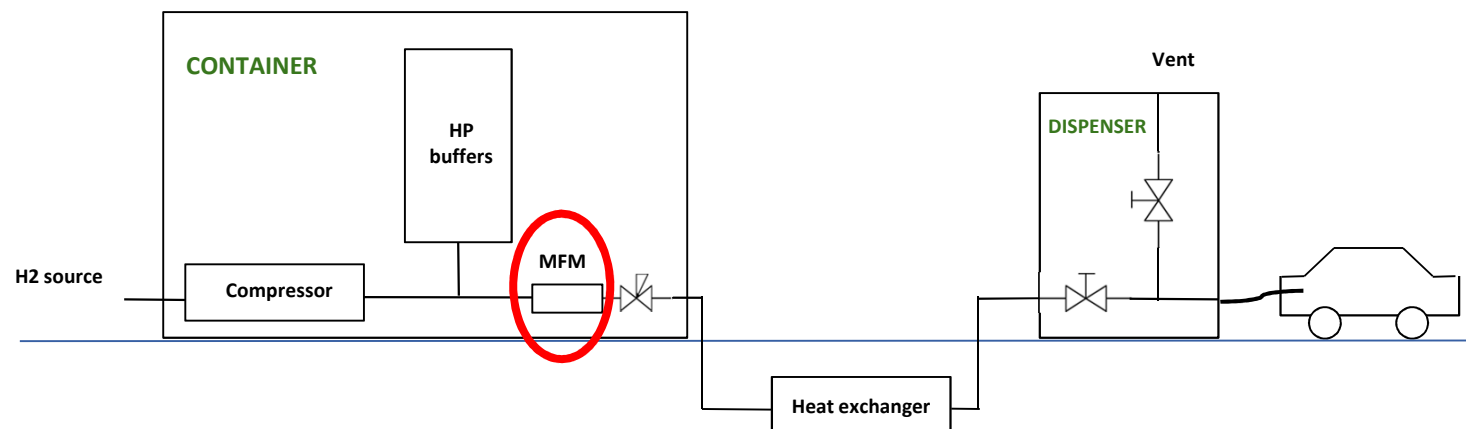


HYDROGEN REFUELLING STATION CALIBRATION

Results from on-site measurements with gravimetric standard



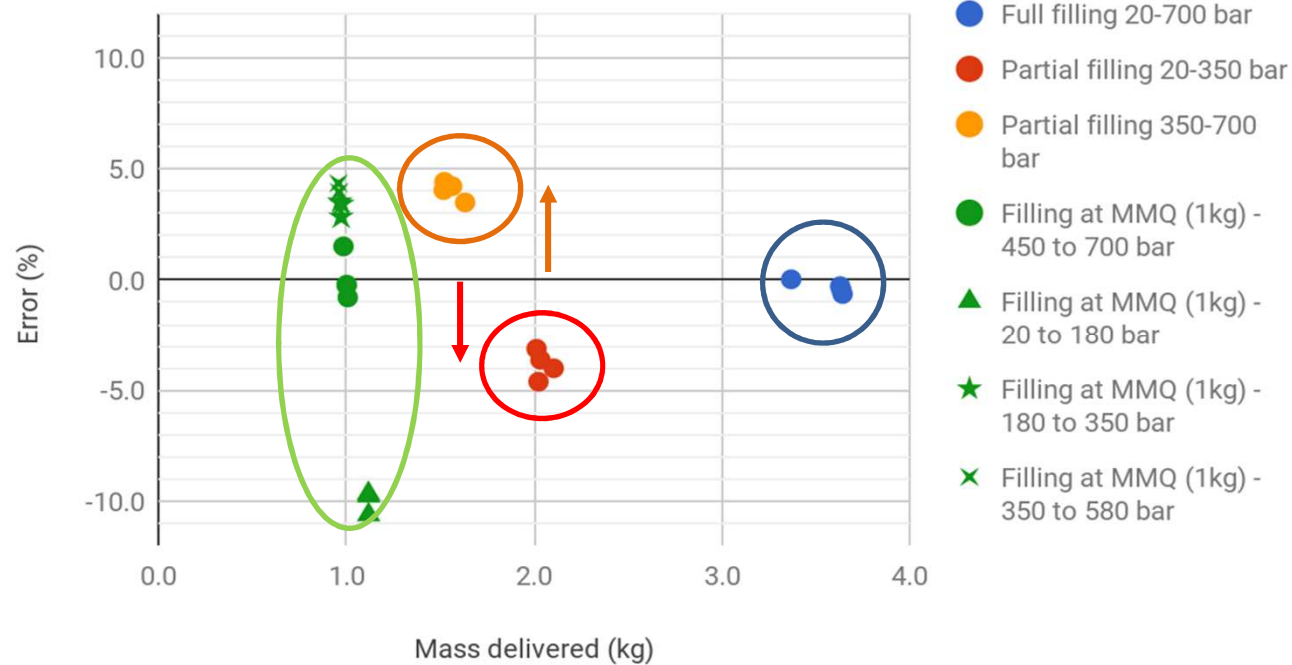
- same configuration (called 1) of the measuring system:



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Results from on-site measurements with gravimetric standard

- Configuration 1: HRS2 (compressed gas) – CFM in the container



- Full filling : good repeatability – around 0
- Partial filling : negative offset (20-350bar)
- Partial filling : positive offset (350-700bar)
- Large scatter at MMQ depending on initial pressure

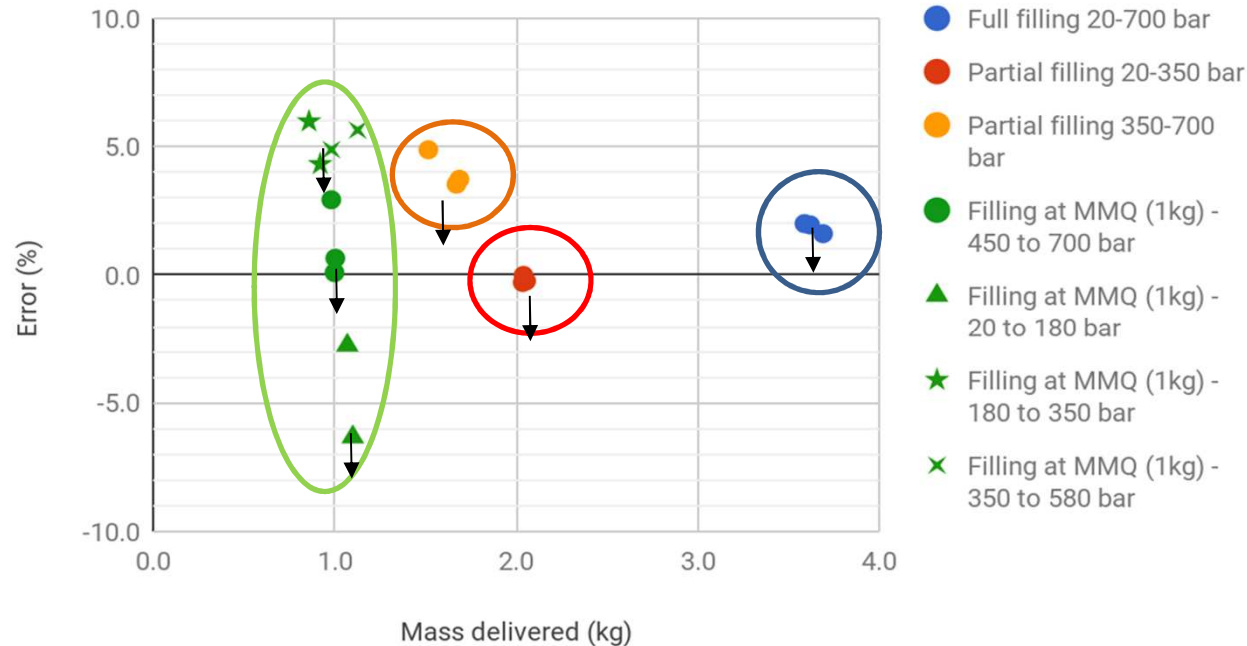


Is this tendency often seen with this configuration 1

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Results from on-site measurements with gravimetric standard

- Configuration 1: HRS1 (compressed gas) – CFM in the container



- The same trends are observed :
- For all fillings : good repeatability – *but offset +2%*

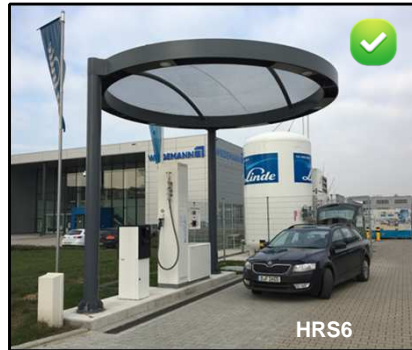
*This could be attributed to k factor in the MFM
Adjustment in Coriolis has not be realized during this test campaign
One adjustment is allowed by the OIML R139*

What about other HRS configuration ?

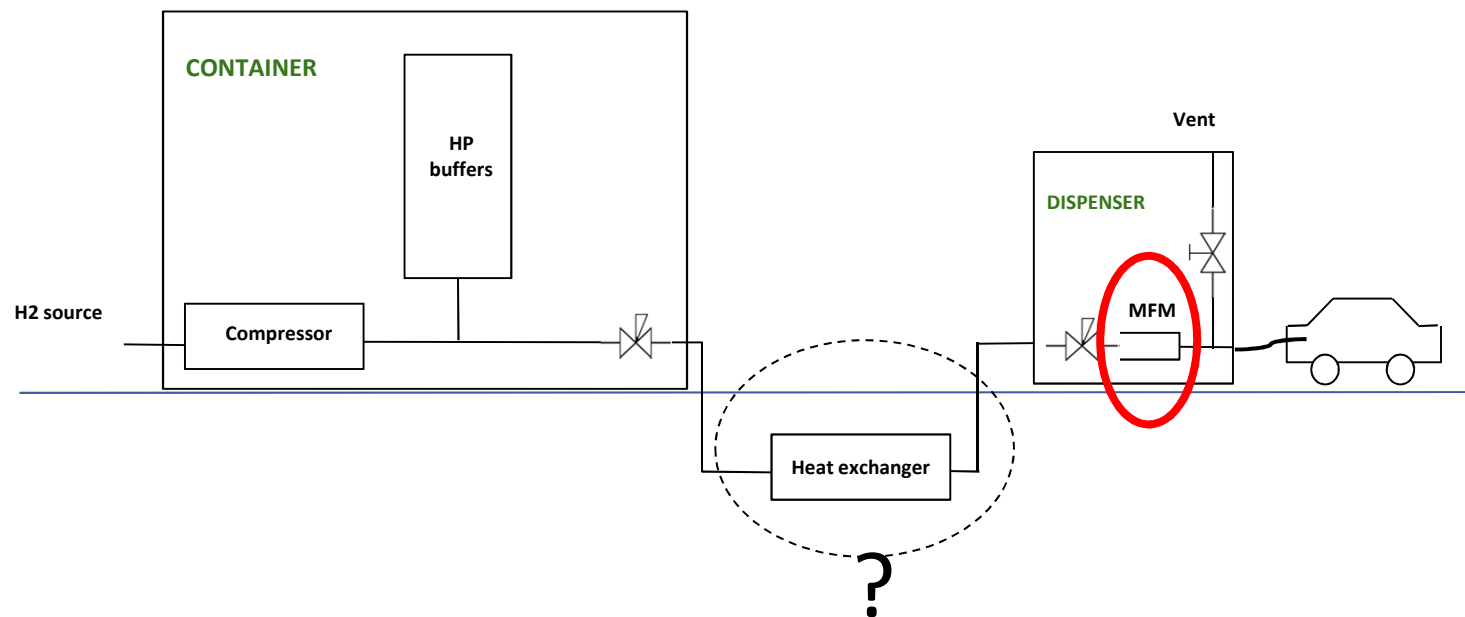


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Results from on-site measurements with gravimetric standard



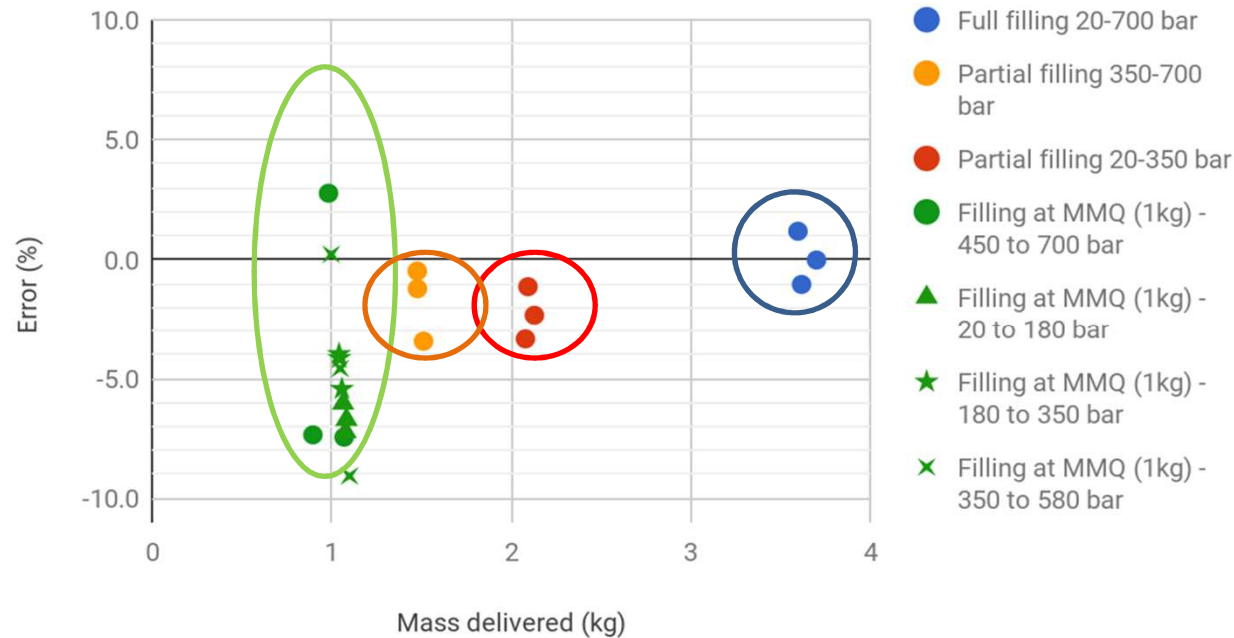
- same configuration (called 2) of the measuring system:



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Results from on-site measurements with gravimetric standard

- Configuration 2: HRS7 (compressed gas) – CFM in the dispenser



- Different results than previous HRS
- More dispersion on the test results (other brand of MFM)
- **Constant deviation seems observed → Icing issue**

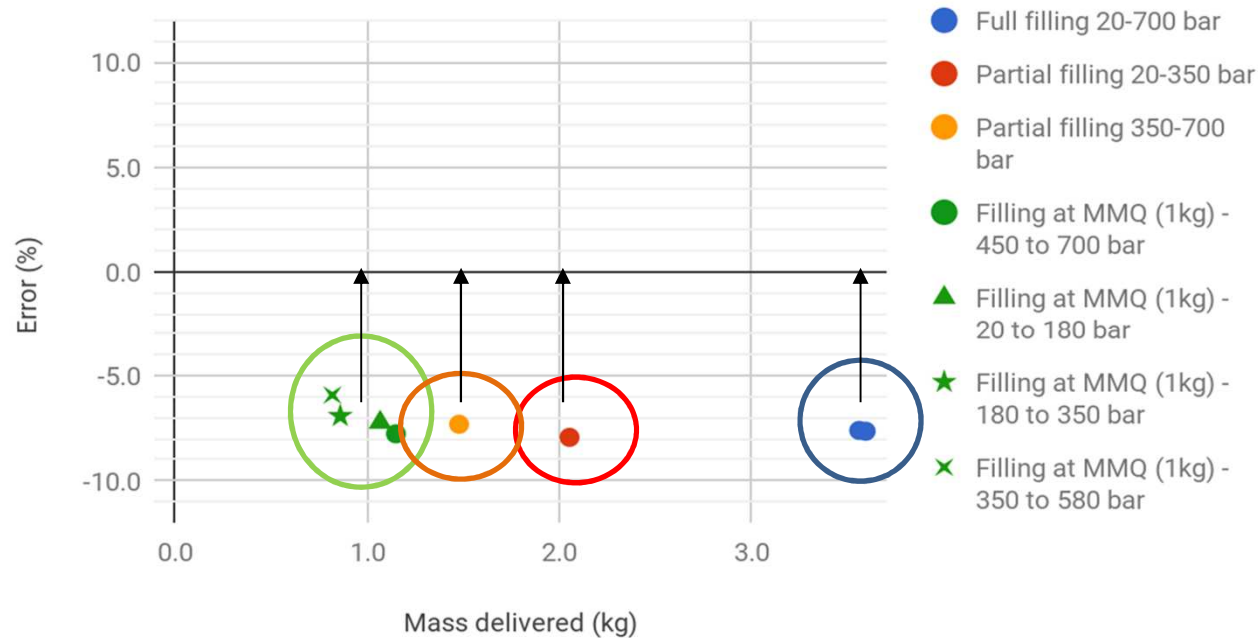
**Remark : weather was bad – high humidity / cold
Venting was taken into account – no indication how**



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Results from on-site measurements with gravimetric standard

- Configuration 2: HRS6 (Liquid H₂) – CFM in the dispenser



- Large negative offset
- Results are centre around -7%
- *If a correction is applied to the CFM, this configuration could reach a class 1.5 in the OIML R139 classification*
- *Only one set before HRS failure.*

Summary of all experiments and accuracy class for HRS



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Results from on-site measurements with gravimetric standard

MEAN VALUES	CONFIGURATION 1					CONFIGURATION 2	
	HRS1 <i>(based on adjusted values)</i>	HRS2	HRS3	HRS4 <i>(based on adjusted values)</i>	HRS5	HRS6 <i>(based on adjusted values)</i>	HRS7
Full fillings 20-700 bar	0,00%	-0,32%	0,52%	0,00%	0,50%	0,00%	0,04%
Partial fillings 20-350 bar (*)	-2,03%	-3,84%	-2,46%	-0,83%	-3,89%	-0,31% (*)	-2,26%
Partial fillings 350-700 bar	2,19%	4,05%	0,72%	1,00%	4,58%	0,31% (*)	-1,71%
Filling at MMQ 450 to 700 bar	-0,63%	0,08%	1,99%	0,50%	4,84%	-0,14% (*)	-4,01%
Filling at MMQ 20 to 180 bar (*)	-6,41%	-10,02%	-9,95%	-1,71%	-6,75% (*)	0,40% (*)	-6,65%
Filling at MMQ 180 to 350 bar (*)	3,29%	3,28%	-5,13%	0,94%	0,51% (*)	0,71% (*)	-4,51%
Filling at MMQ 350 to 580 bar (*)	3,41%	3,69%	-1,08%	0,71%	4,63% (*)	1,70% (*)	-4,47%
CLASS OIML R139	4	4	2	2	4	2	4

Legend:

Green = all values are within the limits (MPE)

Orange = mean value is within the limits (or very close to the limits), but some single values are out of the limits (MPE)

Red = all values are out of the limits (MPE)

(*) *single value*

(*) *tests out of OIML R139:2018 scope*

Explanations for the results

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Results from on-site measurements with gravimetric standard

- **Good reliability of the testing device in ambient conditions** (hot temperatures, moderate wind, cold and humid conditions in winter)
 - Icing phenomenon to be considered and better quantified in the uncertainty budget
- **Influence of the type of MFM:**
 - Three models tested in different configurations
 - Good precision obtained with M1 & M2 MFM (cf. Full fillings) and good overall repeatability
 - Remark on the M3:
 - Dispersion seems more important
 - Further tests required to clearly conclude on the performance of this MFM
- **Influence of the measuring system configuration (distance between the MFM and the nozzle):**
 - **Configuration 2** show lower errors than configuration 1

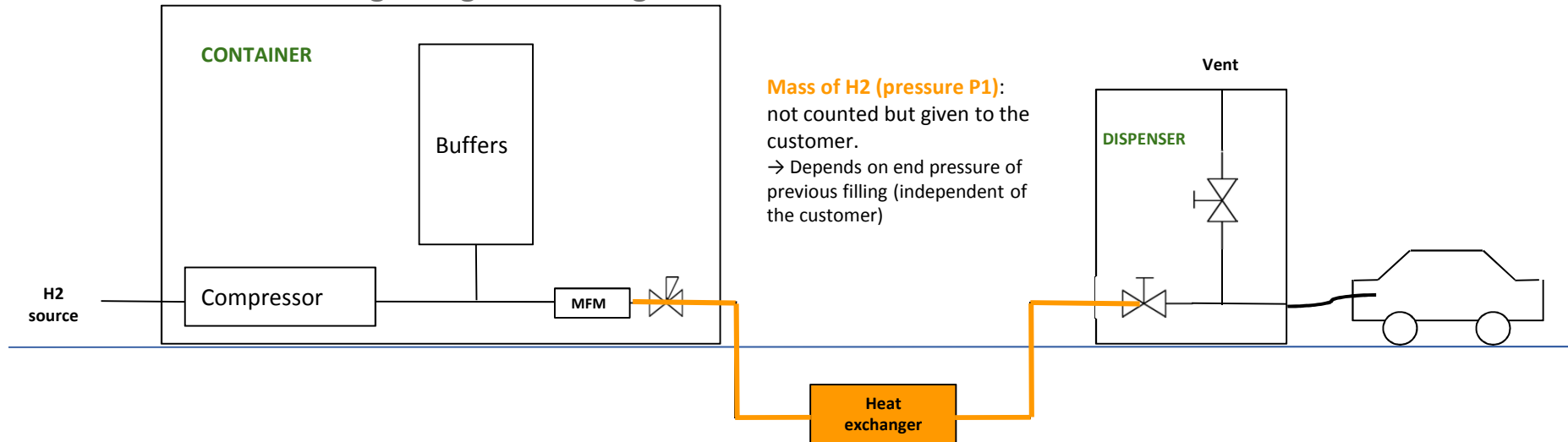
Why?

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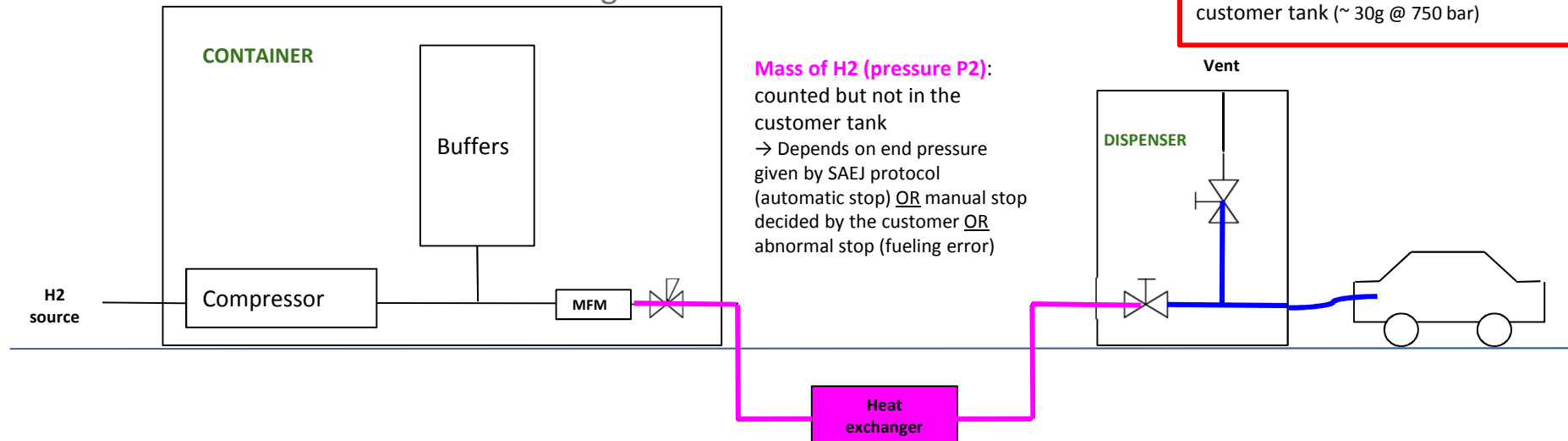
Results from on-site measurements with gravimetric standard

- Influence of distance between MFM and dispenser: Configuration 1**

– Situation at beginning of a fueling



– Situation at the end of a fueling



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Results from on-site measurements with gravimetric standard

• Influence of distance between MFM and dispenser: Configuration 1

- If **P1** ~ **P2**: the customer pays *exactly* the quantity delivered in his tank
 - Initial mass of H2 is replaced by the same quantity at end of fueling

$$m_{\text{delivered}} \sim m_{\text{invoiced}}$$

- If **P1** > **P2**: the customer get *more* hydrogen than the quantity invoiced
 - Initial mass of H2 is replaced by a lower quantity at end of fueling

$$m_{\text{delivered}} > m_{\text{invoiced}} \quad (\text{negative error})$$

- If **P1** < **P2**: the customer get *less* hydrogen than the quantity invoiced
 - Initial mass of H2 is replaced by a higher quantity at end of fueling

$$m_{\text{delivered}} < m_{\text{invoiced}} \quad (\text{positive error})$$

APPLICATION:

- Full fillings 20-700 bar
- MMG (1kg) 450-700 bar
- Partial fillings 20-350 bar
- ▲ MMG (1kg) 20-180 bar
- Partial fillings 350-700 bar
- ★ MMG (1kg) 180-350 bar
- MMG (1kg) 350-580 bar

• Strong influence of the distance between the MFM and the dispenser

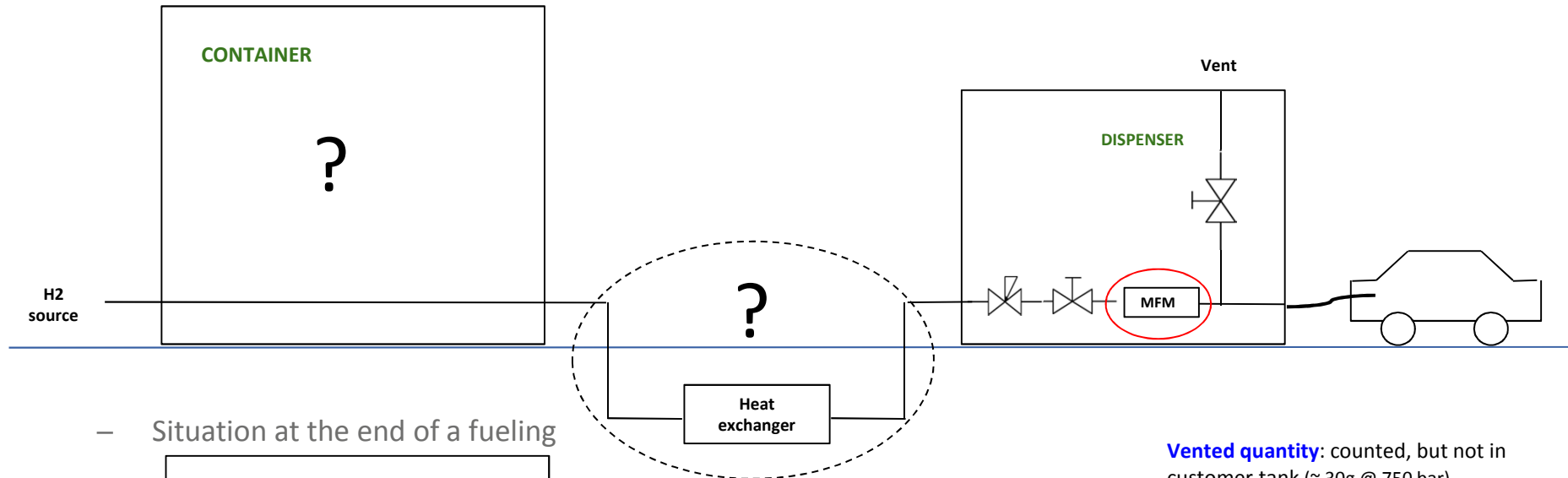
- The longer is the distance (or volume), bigger is the error
- Larger pressure difference in the pipe at beginning and end of fueling leads to a bigger error
 - Example: MMQ fueling at 450 bar and 20 bar initial pressure
- If the volume of piping is known then errors can be calculated and corrected

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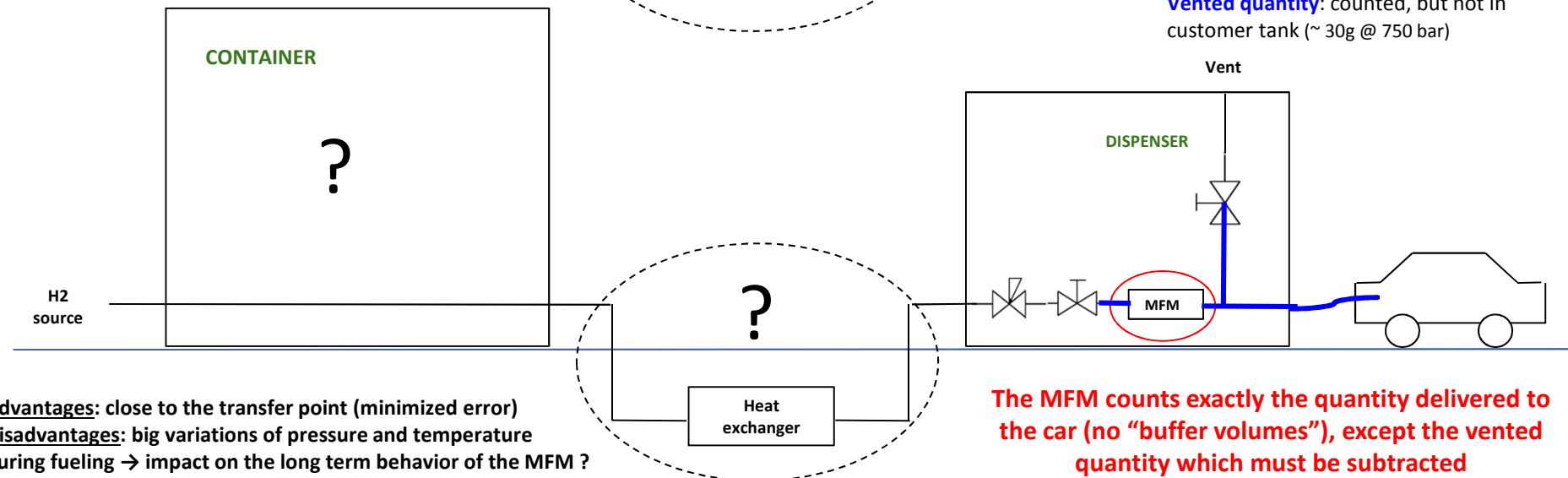
Results from on-site measurements with gravimetric standard

- Influence of distance between MFM and dispenser: Configuration 2

- Situation at beginning of a fueling



- Situation at the end of a fueling



Advantages: close to the transfer point (minimized error)

Disadvantages: big variations of pressure and temperature during fueling → impact on the long term behavior of the MFM ?

The MFM counts exactly the quantity delivered to the car (no “buffer volumes”), except the vented quantity which must be subtracted

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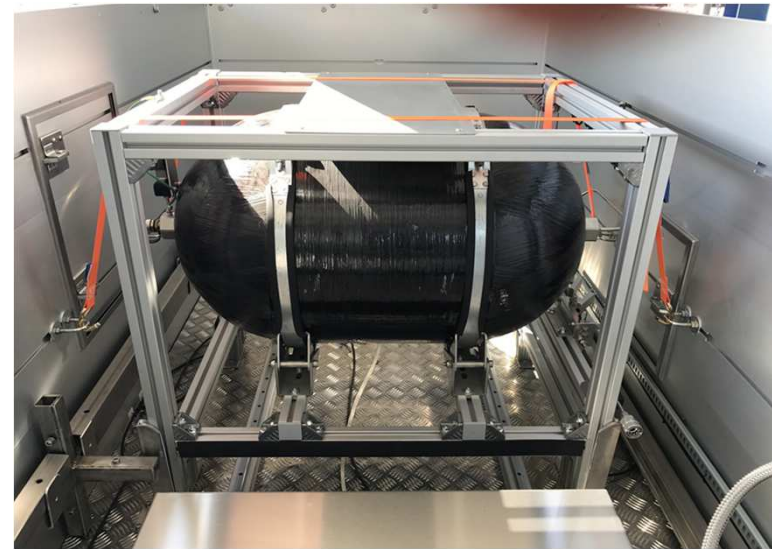
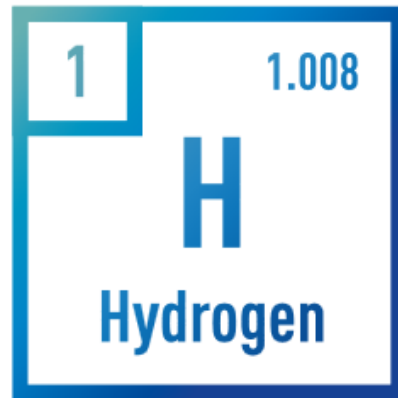
Conclusions and perspectives

- **A primary test bench as been designed and developed for hydrogen refueling station calibration.**
- **An intensive test campaign has been realized in Europe (7 HRS).**
- **The accuracy classes has been found to mainly comply with Class 4 (for existing stations).**
- **The main errors have been measured and some hypothesis have been proposed to understand the difference between two main configurations – Configuration 2 seems more accurate but caution has to be taken regarding operating conditions.**
- **Need to make comparison between primary standard for hydrogen stations and develop new metrological framework for periodic verification to speed up the test campaigning**
- **Need to consider other kind of technologies (bicycles, buses and train) and adapt our reference for these ranges of application.**

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Conclusions and perspectives

- Thank you !



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Backup slides

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Background regarding HRS in Europe

- Hydrogen & Fuel cells have several roles in decarbonizing major sectors of the economy

FUEL CELLS CAN BE USED IN WIDE RANGE OF APPLICATIONS



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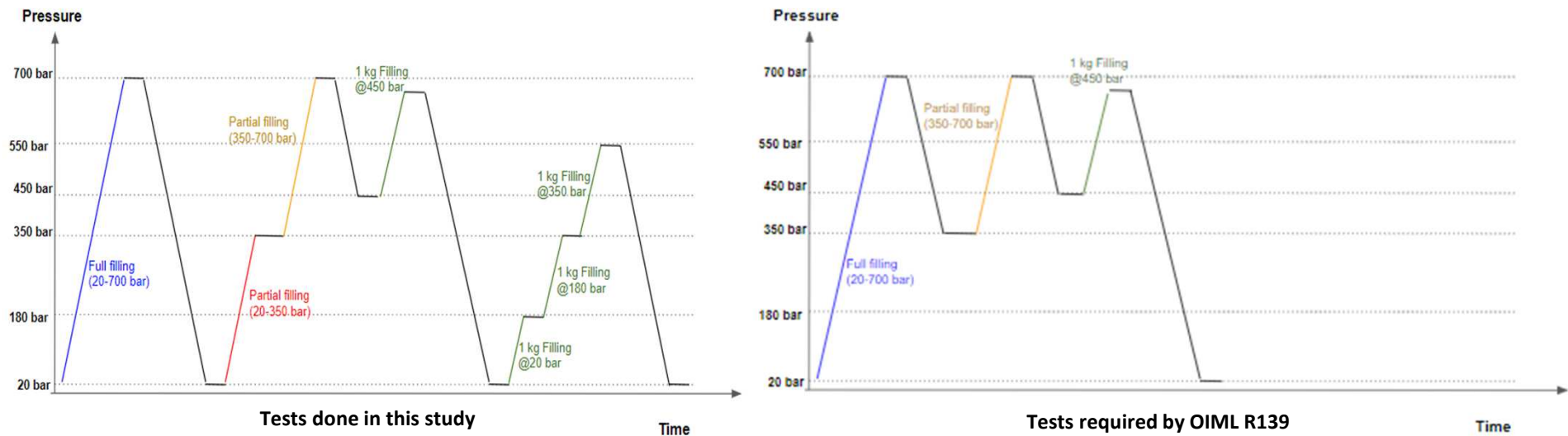
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with different starting pressure (450 bar - 20 bar - 180 bar - 350 bar) Manual stop

- This series of tests is performed **4 times**



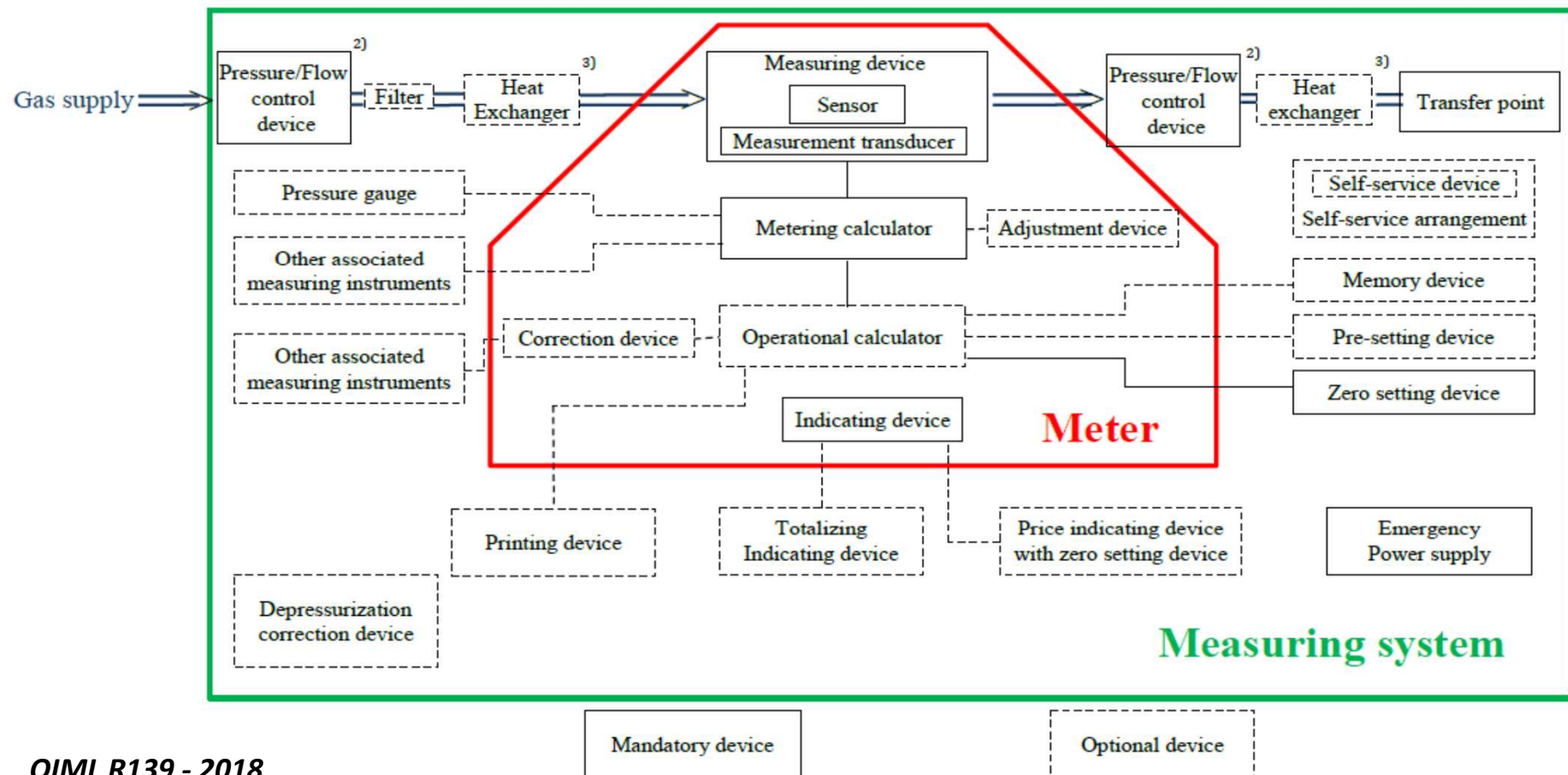
Which kind of technologies have been tested ?

HYDROGEN REFUELLING STATION CALIBRATION

Basic operating principle of a HRS station

- Basic principle and listing of the component: The OIML R139 [2] describes a HRS as a measuring system which should include at least:

- a) meter; b) pressure and/or flow control device; c) emergency power supply; d) transfer point;
- e) gas piping; f) zero-setting device.



HYDROGEN REFUELLING STATION CALIBRATION

primary gravimetric standard (Air Liquide)

- **Testing device designed and manufactured by Air Liquide (in collaboration with Cesame Exadebit)**
 - Certified by PTB (March 2018) as first reference standard for calibration, conformity assessment and verification of hydrogen refueling dispensers
 - Also accepted by LNE (France) and NMI Certin (Netherlands)
 - Fulfills metrological requirements as per OIML R139-2018
 - Uncertainty $U < \frac{1}{3}$ MPE = 0,3%
 - Uncertainty budget defined in collaboration with PTB / LNE / Cesame Exadebit
- **Uncertainty sources**

Ref.	Cause of uncertainty	Uncertainty U(xi)		Probability density function		Type of uncertainty u(xi)	Coefficient of sensitivity		Contribution to the global uncertainty	
		Value	Unit	Type	Divisor		ci	Unit	[ci * u(xi)]*2	in %
B.0	Repeatability of measurements	0,70	g	Rectangular	1,73	4,04E-01	1	g	1,63E-01	13,45%
B.1	Eccentric loads	0,20	g	triangular	2,45	8,16E-02	1	-	6,67E-03	0,55%
B.2.a	Scale resolution when empty	0,20	g	triangular	2,45	8,16E-02	1	-	6,67E-03	0,55%
B.2.b	Scale resolution when loaded	0,20	g	triangular	2,45	8,16E-02	1	-	6,67E-03	0,55%
B.3	Uncertainty of reference weights	0,07	g	Normal	2,00	3,50E-02	1	-	1,23E-03	0,10%
B.4	Scale reliability (temperature effects)	0,20	g	Normal	2,00	1,00E-01	1	-	1,00E-02	0,82%
B.5	Non linearity of the scale	0,50	g	Rectangular	1,73	2,89E-01	1	-	8,33E-02	6,86%
B.6	Air density (ambient conditions)	0,16	g	Rectangular	1,73	9,24E-02	1	-	8,53E-03	0,70%
B.7	Effect of temperature on the scale	0,20	g	Rectangular	1,73	1,15E-01	1	-	1,33E-02	1,10%
B.8	Connection / disconnection influence	0,60	g	Rectangular	1,73	3,46E-01	1	-	1,20E-01	9,89%
B.9	Buyoncy (stability of air density at beginning and end of filling, including vessel expansion)	0,95	g	Rectangular	1,73	5,48E-01	1	-	3,01E-01	24,78%
B.10	Short time drift of balance (temperature effect, wind, balance performance, etc...)	0,40	g	Rectangular	1,73	2,31E-01	2	-	2,13E-01	17,57%
B.11	Water condensation	0,40	g	Rectangular	1,73	2,31E-01	2	-	2,13E-01	17,57%
B.12	Zero stability after depressurization	0,40	g	Rectangular	1,73	2,31E-01	1	-	5,33E-02	4,39%
B.13	Influence of the gouding	0,20	g	Rectangular	1,73	1,15E-01	1	-	1,33E-02	1,10%
Combined uncertainty		$u_c = \sqrt{\sum c_i^2 u_i^2}$		1,35	g	TOTAL =		1,21E+00		
Expanded uncertainty (k = 2)		$U_E (K = 2)$		2,70	g	Class 1,5		Class 2		
Relative expanded uncertainty		$U_r = \frac{U(X)}{X} \times 100$		0,270	%	Criteria: 1/5 of MPE		0,3 0,4		